CLAIM AMENDMENTS

Amend claims:1-13 and added new claims 14 –24.

1. (Currently Amended) A process ~~Process~~ to prepare a base oil having ~~an~~ a paraffin content of between 75 and 95 wt%, the process comprising ~~by~~ subjecting a mixture of a hydroisomerized ~~hydroisomerised~~ Fischer-Tropsch wax and a petroleum derived feed to a catalytic pour point reducing treatment, wherein the petroleum derived feed has an aromatic content of between 0 and 20 wt% and a naphthenic compound content of between 15 and 90 wt% and wherein the fraction of petroleum derived feed in the mixture is higher than 5 wt% and lower than 50 wt%.

2. (Currently Amended) The process of ~~Process according to~~ claim 1, wherein the petroleum derived feed is a bottoms fraction of a fuels hydrocracker.

3. (Currently Amended) The process of ~~Process according to~~ claim 2, wherein the content of sulfur ~~sulphur~~ in the mixed feed to the pour point reducing treatment is below 50 ppm and the content of nitrogen in the mixed feed to the pour point reducing treatment is below 10 ppm.

4. (Currently Amended) The process of claim 1, ~~Process according to any one of claims 1-3,~~ wherein the wax content in the petroleum derived feed is below 30 wt%.

5. (Currently Amended) The process of ~~Process according to~~ claim 4, wherein the pour point of the petroleum derived feed is below -10 °C.

6. (Currently Amended) The process of claim 1, ~~Process according to any one of claims 1-5,~~ wherein the petroleum derived feed has a saturates content of greater than 98 wt% a viscosity index of between 80 and 150 and a sulfur ~~sulphur~~ content of below 0.001 wt%.

7. (Currently Amended) The process of ~~Process according to~~ claim 6, wherein the petroleum derived feed has been obtained in a process ~~involving~~ comprising a hydrofinishing step performed at a hydrogen pressure of greater than 100 bars.

8. (Currently Amended) The process of claim 1, ~~Process according to any one of claims 1-7,~~ wherein the base oil is hydrogenated after performing the pour point reducing treatment such that the content of aromatics is below 1 wt%.

9. (Currently Amended) The process of claim 1, ~~Process according to any one of claims 1-8,~~ wherein the catalytic pour point reducing treatment is a catalytic dewaxing process performed in the presence of a catalyst comprising a Group VIII metal and an intermediate pore size zeolite having pore diameter between 0.35 and 0.8 nm, and a binder.

10. (Currently Amended) The process of claim 1, ~~Process according to any one of claims 1-9,~~ wherein after performing the catalytic pour point reducing treatment hydrogen is separated from the dewaxed effluent, contacted with a heterogeneous adsorbent selective for removing hydrogen sulfide ~~sulphide~~ and recycled to said catalytic pour point reducing treatment.

11. (Currently Amended) The process of ~~Process according to~~ claim 10, wherein the heterogeneous adsorbent is zinc oxide.

12. (Currently Amended) The process of claim 1, ~~Process according to any one of claims 1-11,~~ wherein the hydroisomerized ~~hydroisomerised~~ Fischer-Tropsch wax is obtained by a process comprising ~~means of the following steps~~:

(a) hydrocracking/hydroisomerizing ~~hydroisomerisating~~ a Fischer-Tropsch product, and,

(b) distilling ~~separating by means of distillation~~ the product of step (a) into one or more gas oil fractions and a higher boiling Fischer-Tropsch derived feed.

13. (Currently Amended) The process of ~~Process according to~~ claim 12, wherein the Fischer-Tropsch product used as feed in step (a) is a product wherein the weight

ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms in the Fischer-Tropsch product is at least 0.4 and wherein at least 30 wt% of compounds in the Fischer-Tropsch product have at least 30 carbon atoms.

14. (New) The process of claim 2, wherein the content of sulfur in the mixed feed to the pour point reducing treatment is below 50 ppm and the content of nitrogen in the mixed feed to the pour point reducing treatment is below 10 ppm.

15. (New) The process of claim 2, wherein the wax content in the petroleum derived feed is below 30 wt%.

16. (New) The process of claim 15, wherein the pour point of the petroleum derived feed is below-10 °C.

17. (New) The process of claim 2, wherein the petroleum derived feed has a saturates content of greater than 98 wt% a viscosity index of between 80 and 150 and a sulfur content of below 0.001 wt%.

18. (New) The process of claim 17, wherein the petroleum derived feed has been obtained in a process comprising a hydrofinishing step performed at a hydrogen pressure of greater than 100 bars.

19. (New) The process of claim 2, wherein the base oil is hydrogenated after performing the pour point reducing treatment such that the content of aromatics is below 1 wt%.

20. (New) The process of claim 2, wherein the catalytic pour point reducing treatment is a catalytic dewaxing process performed in the presence of a catalyst comprising a Group VIII metal and an intermediate pore size zeolite having pore diameter between 0.35 and 0.8 nm, and a binder.

21. (New) The process of claim 2, wherein after performing the catalytic pour point reducing treatment hydrogen is separated from the dewaxed effluent, contacted

with a heterogeneous adsorbent selective for removing hydrogen sulfide and recycled to said catalytic pour point reducing treatment.

22. (New) The process of claim 21, wherein the heterogeneous adsorbent is zinc oxide.

23. (New) The process of claim 2, wherein the hydroisomerized Fischer-Tropsch wax is obtained by a process comprising:

(a) hydrocracking/hydroisomerizing a Fischer-Tropsch product, and,

(b) distilling the product of step (a) into one or more gas oil fractions and a higher boiling Fischer-Tropsch derived feed.

24. (New) The process of claim 23, wherein the Fischer-Tropsch product used as feed in step (a) is a product wherein the weight ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms in the Fischer-Tropsch product is at least 0.4 and wherein at least 30 wt% of compounds in the Fischer-Tropsch product have at least 30 carbon atoms.